

Amendments to the Claims:

This listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

1. (Currently Amended) A catalyst, which catalyst comprises silver deposited on a shaped support material having a hollow cylinder geometric configuration such that the length-to-outside diameter ratio of said shaped support material is in the range of from about 0.3 to about 2 and the internal diameter is in the range upwardly to ~~about~~ 30 percent of the outside diameter of said shaped support material.
2. (Original) A catalyst as recited in claim 1, wherein silver is present in a quantity in the range exceeding 15 weight percent of the total weight of the catalyst.
3. (Original) A catalyst as recited in claim 2, wherein silver is present in a quantity in the range of exceeding 20 weight percent to and at most 50 weight percent, of the total weight of the catalyst.
4. (Original) A catalyst as recited in claim 1, wherein the support material has a water absorption exceeding 40%.
5. (Original) A catalyst as recited in claim 1, wherein the support material has a surface area in the range of from 0.03 m²/g to 10 m²/g.
6. (Original) A catalyst as recited in claim 1, wherein the support material has a water absorption in the range of from 42.5% to 80%, and a surface area in the range of from 0.5 m²/g to 5 m²/g.
7. (Currently Amended) A catalyst as recited in claim 1, wherein the length-to-outside diameter ratio is in the range of from about 0.5 to about 1.6 and the ratio of internal diameter to outside diameter is in the range of from ~~about~~ 0.01 to ~~about~~ 0.25.
8. (Currently Amended) A catalyst as recited in claim 7, wherein the length-to-outside diameter ratio is in the range of from about 0.9 to about 1.1 and the ratio of internal diameter to outside diameter is in the range of from ~~about~~ 0.02 to ~~about~~ 0.2.
9. (Original) A catalyst as recited in claim 1, wherein the outside diameter is in the range of from 4 to 16 mm, and the bore diameter is smaller than 3.5 mm.
10. (Original) A catalyst as recited in claim 1, wherein the outside diameter is in the range of from 5 to 12 mm, and the bore diameter is in the range of from 0.1 to 3 mm.
11. (Original) A catalyst as recited in claim 1, wherein the bore diameter is in the range of from about 0.2 mm to about 2 mm.

12. (Original) A catalyst as recited in claim 1, wherein the catalyst further comprises a promoter component comprising a rare earth metal, magnesium, rhenium, or an alkali metal.

13. (Original) A catalyst as recited in claim 1, wherein the catalyst further comprises a promoter component comprising rhenium, an alkali metal selected from lithium, potassium, rubidium and cesium, and, in addition, a rhenium copromoter comprising sulfur, molybdenum, tungsten or chromium.

14. (Currently Amended) A method, comprising:

providing a shaped support material having a geometric configuration such that the length-to-outside diameter ratio is in the range of from about 0.3 to about 2 and the internal diameter is in the range upwardly to about 30 percent of the outside diameter of said shaped catalyst support; and

depositing silver on the shaped support.

15. (Original) A method as recited in claim 14, comprising depositing on the support, in addition to silver, a promoter component comprising rhenium, and a rhenium copromoter comprising sulfur, molybdenum, tungsten or chromium, wherein the rhenium copromoter is deposit prior to or simultaneous with the deposition of silver, and rhenium is deposited after at least a portion of the silver has been deposited.

16. (Withdrawn) A packed catalyst bed, which packed catalyst bed is formed from catalyst particles comprising silver supported on a shaped support, which catalyst bed has a silver loading of at least 150 kg silver/m³ catalyst bed.

17. (Withdrawn) A packed catalyst bed as recited in claim 16, wherein the silver loading is in the range of from 170 to 800 kg silver/m³ catalyst bed.

18. (Withdrawn) A packed catalyst bed as recited in claim 17, wherein the silver loading is in the range of from 200 to 600 kg silver/m³ catalyst bed.

19. (Withdrawn) A process for manufacturing ethylene oxide, which process comprises: contacting, under suitable epoxidation process conditions, a feed stream, comprising ethylene and oxygen, with the catalyst of claim 1, or with the catalyst bed of claim 18.

20. (Withdrawn) A process as recited in claim 19, wherein the feed stream which is contacted with the catalyst, and which comprises ethylene and oxygen, has a concentration of carbon dioxide of at most 4 mole-%, in particular at most 2 mole-%, more in particular at most 1 mole-%, relative to the total feed.

21. (Withdrawn) A method of using ethylene oxide for making ethylene glycol, an ethylene glycol ether or an 1,2-alkanolamine comprising converting ethylene oxide into

ethylene glycol, the ethylene glycol ether, or the 1,2-alkanolamine, wherein the ethylene oxide has been obtained by the process for preparing ethylene oxide as recited in claim 19.